AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

LISTING OF CLAIMS:

1-8. (cancelled)

9. (currently amended) Method for the selective catalytic reduction of nitrous oxide (N_2O) in the presence of a solid catalyst, with the addition of a saturated hydrocarbon as a reducing agent, wherein the catalyst used is an iron-containing zeolite promoted with at least one precious metal selected from the group consisting of ruthenium, rhodium, palladium and gold; the catalyst thereby comprising a zeolite which contains at least one combination of metals selected from the group consisting of iron and ruthenium, iron and rhodium, iron and palladium and iron and gold, for the catalytic reduction of nitrous oxide.

10. (previously presented) The method according to claim 9, wherein the catalyst is promoted with a combination of two or more precious metals selected from the group consisting of ruthenium, rhodium, palladium and gold.

11. (previously presented) The method according to claim 9, wherein the reducing agent used is natural gas or methane (CH_4) or propane (C_3H_8) or LPG (C_3H_8/C_4H_{10}).

12. (previously presented) The method according to claim 11, wherein a combination of reducing agents is used.

13. (previously presented) The method according to claim 9, wherein the concentration of the reducing agent is set in such a way that the hydrocarbon/N_2O molar ratio is in the range from 0.2 to 20.

14. (previously presented) The method according to claim 13, wherein the molar ratio of hydrocarbon to N_2O ranges from 0.5 to 5.

15. (previously presented) The method according to claim 9, wherein the reduction takes place at an inlet temperature of less than 400°C.

16. (previously presented) The method according to claim 9, wherein the reduction results in an emission of carbon monoxide (CO) and of hydrocarbon, which is in each case separately less than 100 ppmv.

17. (previously presented) The method according to claim 9, wherein the reduction takes place at a pressure between 1 and 50 bar absolute.

18. (currently amended) Method for the selective catalytic reduction of nitrous oxide (N_2O) from an industrial gas stream containing N_2O, O_2, H_2O, NO_x and optionally sulfur, which comprises:

- providing a catalyst comprising an iron-containing zeolite promoted with at least one precious metal selected from the group consisting of ruthenium, rhodium, palladium and gold; the catalyst thereby comprising a zeolite which contains at least

one combination of metals selected from the group consisting of iron and ruthenium, iron and rhodium, iron and palladium and iron and gold; and

- contacting the gas stream with the catalyst in the presence of a saturated hydrocarbon as a reducing agent for the catalytic reduction of nitrous oxide.

19. (previously presented) The method according to claim 18, wherein the catalyst is promoted with a combination of two or more precious metals selected from the group consisting of ruthenium, rhodium, palladium and gold.

20. (previously presented) The method according to claim 18, wherein the reducing agent used is natural gas or methane (CH_4) or propane (C_3H_8) or LPG (C_3H_8/C_4H_{10}).

21. (previously presented) The method according to claim 20, wherein a combination of reducing agents is used.

22. (previously presented) The method according to claim 18, wherein the concentration of the reducing agent is set in such a way that the hydrocarbon/N_2O molar ratio is in the range from 0.2 to 20.

23. (previously presented) The method according to claim 22, wherein the molar ratio of hydrocarbon to N_2O ranges from 0.5 to 5.

24. (previously presented) The method according to claim 18, wherein the reduction takes place at an inlet temperature of less than 400°C.

25. (previously presented) The method according to claim 18, wherein the reduction results in an emission of carbon monoxide (CO) and of hydrocarbon, which is in each case separately less than 100 ppmv.

26. (previously presented) The method according to claim 18, wherein the reduction takes place at a pressure between 1 and 50 bar absolute.